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(54) **Integrated ceramic micro-chemical plant**

Integrierte keramische mikro-chemische Anlage

Installation micro-chimique en céramique

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**WO-A-96/03206** **WO-A-96/04516**  
**DE-A- 3 926 466** **US-A- 3 881 701**  
**US-A- 5 265 327**

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**EP 0 870 541 B1**

## Description

[0001] The present invention relates to an integrated ceramic micro-chemical plant which can be used to mix, react or analyze chemicals.

[0002] Micro-engineering is a rapidly growing field which will impact on many applications over the coming years. Three-dimensional micro-engineered devices and systems involving silicon planar technology can be produced with features from one to a few hundred microns having tolerances in micron or as small as sub-micron level. Most of the current micro-engineering technologies are evolved from the adaptation of thin films, photolithographic and etching technologies generally applied to silicon wafers on which silicon mono oxide, silicon dioxide, silicon nitride and the like thin films are deposited and etched thereafter yielding planar configurations

[0003] Advances have been made to study chemical processes based on microfluidic systems technology using planar structures on silicon chips. Predictive flow modeling has also been developed to realize the benefits from the microfluidic technology.

[0004] The performance of chemical processing is strictly governed by the mass transport and sometimes thermal transport properties of the system. It is therefore essential to understand how miniaturization affect the chemical processes. Laminar flow of an ideal fluid in a tube or channel is well characterized. Pfahler et al have demonstrated in an experiment using channels of various geometry on silicon wafers that there is an agreement between experiment and theory concluding that the conventional Hagen-Poiseuille equation is obeyed down to a scale of few microns. Laminar volume flow per unit time,  $Q_f$ , of an ideal fluid in a circular pipe is described by the Hagen-Poiseuille equation:

$$Q_f = \frac{\pi}{8\mu_f} \cdot \frac{dp}{dx} r^4$$

where  $\mu_f$  and  $r$  are the fluid viscosity and tube radius respectively,  $dp/dx$  is the pressure gradient along the x-direction of flow.

[0005] As the channel widths are reduced, the fluid flow becomes more laminar which provides control over the distribution of material and that dictates that liquid mixing be achieved by diffusion or other molecular migration processes rather than by turbulence. This problem of mixing can be solved by commercially available software packages on computational fluid dynamics. A measure of degree of mixing,  $F$ , can be estimated from the expression  $F = Dt/l^2$ , where  $D$  is a reactant diffusion constant,  $t$  is contact time allowed for mixing and  $l$  is distance across a reactant stream. Quantitatively, mixing may be defined as substantial to nearly complete for  $F$  values from 0.1 to 1. Typical near complete mixing of two liquids in 1 second corresponds to channel widths of 100  $\mu\text{m}$ .

[0006] Similar arguments apply to heat transfer in micro-channels under laminar flow conditions. Understanding of this laminar heat flow process is useful in designing and building micro heat exchangers and chemical micro-reactors.

[0007] The current planar silicon technologies are inadequate for the fabrication of an integrated and self-contained micro-chemical plants having embedded structure and unitary construction.

[0008] WO-A 96/03206 discloses an integral structure for chemical processing, particularly high-speed mixing and chemical reacting, in which a plurality of laminae are joined together and having inlet and outlet ports connected by a plurality of intersecting channels formed therethrough which accommodate the passage of one or more chemicals.

[0009] The integral structure does not comprise neither at least four ceramic layers, nor an analyzing chamber in the fourth layer.

[0010] It is an object of the present invention to provide an integrated micro-ceramic chemical plant.

[0011] It is another object to provide an integrated micro-ceramic chemical plant which is less than one thousandths the size of an average industrial chemical plant.

[0012] These objects are achieved in an integrated micro-ceramic chemical plant having a unitary ceramic body formed from multiple ceramic layers in the green state which are sintered together comprising:

(a) the unitary ceramic body defining a mixing chamber and passage means for providing communication with the mixing chamber so that two or more fluids may be delivered to such mixing chamber for mixing or reacting chemicals in the fluids; and

(b) the unitary ceramic body including means for delivering the mixed or reacted chemicals to exit from the unitary ceramic body.

[0013] Integrated micro-ceramic chemical plants have a number of advantages:

1. By reducing the dimensions of the plant it is possible to ensure good mixing in a short time without the need to introduce turbulence. For those liquids which require turbulence mixing can also be incorporated in the plant.

2. More efficient thermal control is possible because of large surface to volume ratio. Since relatively small quantities of chemicals are used in the micro-channels at any given time, the risk of chemical explosion is also reduced. It is also possible to shut down the process very quickly.

3. Catalytic reaction can be enhanced by providing a large surface to volume ratio by introducing reactants to catalytic surfaces. Additionally, the precise geometry of a micro-ceramic chamber or channel can be used to control the contact time and the

chemical reaction process.

4. The integrated micro-ceramic chemical plants help accurate monitoring of the process *in situ* facilitating process parameters changes.

5. Scaling up the production process is possible by incorporating an array of integrated micro-ceramic chemical plants rather than increasing the volume of the reaction vessels which very often necessitates the change in process parameters.

6. The well defined geometry and ceramic materials selection of the integrated micro-ceramic chemical render them an ideal research tool to study chemical processes.

7. Since the integrated micro-ceramic chemical plants are small in size they can be easily and cost-effectively transported from one place to another.

8. Integrated micro-ceramic chemical plants can withstand harsher chemical environment and higher operating temperatures than those made using conventional silicon technologies.

9. Unlike the conventional silicon technologies, three dimensional embedded channels and other complicated features can be produced within a ceramic body using micro-molding techniques.

10. One of the greatest attributes of integrated micro-ceramic chemical plant is that the emission of effluent gases and discharge of toxic chemical by-products can be effectively controlled enabling the integrated micro-ceramic chemical plant to be environmentally compatible.

Fig. 1 is an exploded perspective of an integrated micro-ceramic chemical plant in accordance with the present invention;

Fig. 2 is a perspective of the first ceramic layer of the unitary ceramic body shown in Fig. 1;

Fig. 3a is a perspective of the second ceramic layer from the top of the unitary ceramic body showing mixing channels;

Fig. 3b is a cross-sectional end view of Fig. 3;

Fig. 4a is a perspective of the third ceramic layer from the top of the unitary ceramic body showing reaction chambers;

Fig. 4b is a cross-sectional view along the lines 4A-4A of Fig. 4a;

Fig. 4c is a cross-sectional view along the line 4B-4B of Fig. 4a;

Fig. 5a is a partial perspective of the reaction chamber in Fig. 4a and provided with an electrical stirrer;

Fig. 5b is a partial perspective of the reaction chamber in Fig. 4a with embedded helical coil for heating;

Fig. 5c is a perspective of a reaction chamber in Fig. 4a showing a ceramic filter;

Fig. 6 is a perspective of the fourth ceramic layer from the top of the unitary ceramic body showing chambers for analyzing the chemical

reaction processes; and

Fig. 7 is a perspective of the fifth ceramic layer residing at the bottom of the unitary ceramic body showing chambers for retrieving the products and also a heat unit for heating the ceramic body.

[0014] Referring to Fig. 1, a perspective is illustrated of an unitary ceramic body 10 which includes five different ceramic layers. The individual ceramic layers are initially in the green state, but are sintered together to form the unitary ceramic body 10. The top ceramic layer 20 of the unitary ceramic body 10 has passageways 12 and 14 on opposite sides of the unitary ceramic body 10. (See FIG. 2) The passageways 12 and 14 are adapted to receive fluids containing chemicals which are to be mixed, reacted and analyzed in accordance with the present invention. It is to be noted that the top ceramic layer 20 may contain more than two passageways 12 and 14. The passageways 12 lead directly to the second ceramic layer 30 which includes mixing chamber 31 and mixing channels 26. Alternatively, the passageways 14 can lead directly to the third ceramic layer 40 in order to bypass the mixing chamber 31. The third ceramic layer 40 defines reaction chambers 44, 46, 48. (See Fig. 4a) Referring to Fig. 1 again, the fourth ceramic layer 100 includes analyzing channels 72 for analyzing the chemical process. The bottom or fifth ceramic layer 200 includes a discharging channel 80 for discharging the reacted product. Also embedded heating coil 84 is formed in the fifth ceramic layer 200 for heating the unitary ceramic body 10. It will be understood that the embedded heating coil 84 does not necessarily have to be placed in the fifth ceramic layer 200 as long as it heats the entire unitary ceramic body 10.

[0015] The present invention involves an integrated micro-ceramic chemical plant. When the term "micro" is used it refers to the fact that the features within the chemical plant have dimensions of about 100  $\mu\text{m}$  or less. The unitary ceramic body 10 is formed by multiple ceramic layers in the green state which are sintered together. These layers can typically have dimensions 10 to 100 mm wide, 10 to 100 mm long, and 1 to 10 mm thick.

[0016] The use of the term "green" means that when particulate ceramic powder, preferably mixed with an organic binder is subjected to uniform compacting forces in order to provide an unsintered preform which has uniform density. One particular effective material is a tetragonal zirconia ceramic powder that can be micro-molded to form the layer by standard methods such as injection molding, gel casting, tape casting, dry pressing or cold isostatic pressing. Other ceramic materials which can be used are ceramics such as  $\text{Al}_2\text{O}_3$ ,  $\text{ZrO}_2$ ,  $\text{AlN}$ ,  $\text{BN}$ ,  $\text{MgO}$ ,  $\text{Al}_2\text{O}_3\text{-ZrO}_2$ ,  $\text{SiC}$ ,  $\text{Si}_3\text{N}_4$  and other oxide and non-oxide ceramics and their composites thereof.

[0017] The features within each layer such as chambers, channels and passageways can be formed as fol-

lows:

(a) features like feed-through, through-holes, mixing chambers and reaction chambers can be formed in each layer in the green stage by incorporating those features in the mold. Approximately, 20% to 50% larger features must be made to account for shrinkage during sintering. The amount of shrinkage depends on the relative amount of organic binders in the ceramic mixture. Typically, 2% to 5% by weight organic binders are added for compaction processes such as cold isostatic pressing and dry pressing. On the other hand, 10% to 40% by weight organic binders are added for compaction processes such as gel casting, tape casting and injection molding.

(b) features like embedded helical coils and heating coils can be formed by placing sacrificial members comprising organic polymers which are burned away during the sintering process.

(c) features like microchannels can be formed by embedding sacrificial member which burn away during sintering or can be incorporated in the molding tools.

During the sintering process the green ceramic layers shrink. Provision must be made to compensate for this shrinkage.

[0018] Referring to Fig. 2, a perspective illustrates a top ceramic layer 20 including passageways 12 and 14 arranged in two different rows. A plurality of passageways 12 forming a row are placed directly on through-holes 13 and a plurality of passageways 14 forming another row are placed directly on through-holes 15. A row of through-holes 15 (for clarity of illustration, only two are shown) are connected to a row of through-holes 29 in the mixing chamber (second ceramic layer 30) and feeds into the distributing chambers 43 which are connected to a distributing manifold 48a which are connected to the reaction chambers 44, 46, 48. The passageways 12 and 14 can be made by extruding ceramic powder compounded with organic binders. The top ceramic layer 20 containing the through-holes 13 and 15 can be fabricated by dry pressing ceramic powder. The top ceramic layer 20 and the passageways 12 and 14 can be sintered separately or at the same time, whereby the passageways 12 and 14 will be bonded onto the top ceramic layer 20 during sintering. If the top ceramic layer 20 and the passageways 12 and 14 forming structures are sintered separately they can be brazed or epoxy bonded later.

[0019] In Fig. 3a, a perspective is illustrated of the second ceramic layer 30 which contains mixing chamber 31 for receiving fluids containing the chemicals from the top ceramic layer 20. A plurality of channels 24 exiting from the mixing chamber 31 merge and form a single mixing channel 26 which can be configured to have straight, serpentine, complex, wavy and angular forms

or shapes. A row of through-holes 29 (but only two are shown) are arranged in the second ceramic layer 30 to communicate with the passageway 14 in the top ceramic layer 20. The mixing channel 26 leads to a through-hole 28 which merges into the third ceramic layer 40. Fig. 3b represents a sectional end view of the second ceramic layer 30 in which mixing channel 26 is configured to have circular shape. The mixing chamber 31 can be of rectangular, oval, circular or any convenient shape. The through-hole 28 is directly connected to a distributing chamber 42 in the third ceramic layer 40.

[0020] Referring to Fig. 4a, a perspective is shown of the reaction chambers 44, 46, 48 of the unitary ceramic body 10. The third ceramic layer 40 includes a plurality of communicating fluid channels 45 and 47 and a distributing manifold 48a. The through-hole 28 feeds the fluids containing chemicals to the distributing chamber 42 from where it is distributed to reaction chambers 44, 46 and 48. Additional fluids containing chemicals which do not require to be mixed in the mixing channel 26 can be fed directly to the distributing chamber 43. The reaction chambers 44, 46, 48 can be individually equipped with heaters, stirrers or filters as will be described later. The chemicals from the distributing chamber 43 are distributed individually or combined through the distributing manifold 48a to the reaction chambers 44, 46, 48. The chemicals can be delivered to the reaction chambers 44, 46, 48 separately or sequentially as the processing demands. For separate distribution to the reaction chambers 44, 46, 48 one or two way valves can be incorporated in the channels 45. Alternatively, the chemicals can bypass the reaction chambers 44, 46, 48 and be fed directly to a temporary holding tank 50 via a channel 47. The reaction chambers 44, 46, 48 include the feed-through holes 52 and 54 for inserting thermocouples and stirrers, respectively. The holding tank 50 includes a feed-through hole 56 into which a thermocouple can be inserted. Alternatively, a flow interrupter can also be inserted through a hole 57 for holding the fluid in that chamber. Figs. 4b and 4c are cross-sectional end views along the lines 4A-4A and 4B-4B respectively of Fig. 4a. The fourth ceramic layer 100 which is in communication with the holding tank 50 can either be fully or partially exposed to the next chamber. Also, as shown in Fig. 4c in the bottom of the holding tank 50 there is provided a through-hole 57 which can be opened or closed manually or automatically as desired.

[0021] Referring to Fig. 5a, a partial perspective is shown of the reaction chamber. It is to be noted that the reaction chambers 44, 46 and 48 can have circular, rectangular, square, oval or any desirable geometric shapes. A feed-through hole is provided on one side of the reaction chamber 48 to insert an electrically operated stirrer for mixing reactants with turbulent motion. The stirrer 61 can be constructed from stainless steel having collapsible blades 59 made from plastic or stainless steel.

[0022] Referring to Fig. 5b, a partial perspective is

shown of the reaction chamber 44 having an embedded helical coil structure 63 which can be connected to an external power supply (not shown) through the electrically conductive pad 60 for heating the reaction chamber 44. There is also provided a feed-through hole 52 for inserting thermocouples or other analytical devices to monitor the chemical reaction process. The construction of the embedded helical coil structure 63 is achieved by molding the green ceramic with a sacrificial plastic coil or coils made from refractory metals such as W, Ta and Mo. Plastic sacrificial coil burn off during sintering in air. Refractory metal sacrificial coils are etched away with NaOH or ammonium hydroxide after the ceramic plant has been sintered.

[0023] Referring to Fig. 5c, a perspective is shown of the reaction chamber 46 being formed with compartments comprising a filter 62 which is also made from a selected ceramic and formed as an integral part of the unitary ceramic body 10. A through-hole 64 is provided at the bottom of the reaction chamber 46 to retrieve the solid precipitates. The through-hole 64 can be continuous through the successive layers to the fifth ceramic layer 200. Another fit through hole 66 is provided in the chamber to insert thermocouples and their connecting wires. It is to be noted each reaction chamber 44, 46 and 48 can be formed with compartments comprising one or more than one filters as an integral part of the unitary ceramic body 10.

[0024] Referring to Fig. 6, a perspective is shown of the analyzing chamber 100 of the unitary ceramic body 10. A holding tank 70 is strategically placed under the holding tank 50 (Fig. 4a) of the third ceramic layer 40. The holding tank 50 feeds the analyzing channels 72 which are provided with feed-through holes 74, 76 on both side of the fourth ceramic layer 100. Analytical tools such as mass and optical spectroscopy can be provided and communicate with the exterior of the unitary ceramic body 10 via fiber optic transmission. At the other end of the channels away from the holding tank 70 are located through-holes 78 to deliver the chemicals to the fifth ceramic layer 200.

[0025] Referring to Fig. 7, a perspective is shown of the fifth ceramic layer 200 including discharging channel 80 for receiving chemicals through holes 78 to finally to distribution vessels through a passageway 82. The fifth ceramic layer 200 is also provided with integrated heating elements having embedded heating coil 84 in order to heat the unitary ceramic body 10. The embedded heating coil 84 can be made from ceramic materials such as  $\text{MoSi}_2$ ,  $\text{TiB}_2$  and  $\text{ZrB}_2$ . The electrical leads 86 for the embedded heating coil 84 are located at the side of the fifth ceramic layer 200 and are an integral part of it. In order to monitor and control the temperature, a feed-through hole 90 is provided which protrudes at an angle from outside to the surface of the fifth ceramic layer 200.

## Claims

1. An integrated micro-ceramic chemical plant having a multiple layer unitary ceramic body (10) formed from at least four ceramic layers in the green state which are sintered together comprising :
  - (a) the first ceramic layer (20) being formed with passageways (12, 14) for dispensing at least two fluids containing chemicals;
  - (b) the second ceramic layer (30) including a second layer mixing chamber (31) being in communication with passageways (12,14) for mixing the fluids containing chemicals;
  - (c) the third ceramic layer (40) including a third layer reaction chamber (44, 46, 48) for reacting the chemicals in the fluids ; and
  - (d) the fourth ceramic layer (100) including a fourth layer analyzing chamber for use in analyzing the result of the chemical reactions, wherein the integrated micro-ceramic chemical plant further includes a fifth ceramic layer (200) residing at the bottom portion of the said unitary ceramic body (10) and defining means for delivering the mixed or reacted chemicals to exit from the unitary ceramic body (10).
2. The integrated micro-ceramic chemical plant of claim 1 further including a heating unit disposed in the unitary ceramic body (10) for heating such unitary ceramic body (10).
3. The integrated micro-ceramic chemical plant of claim 1 wherein the second, third, fourth and fifth ceramic layers include capillaries or channels of circular cross-section.

## Patentansprüche

1. Integrierte mikrokeramische, chemische Anlage mit einem eine Vielzahl von Schichten aufweisenden unitären keramischen Körper (10), der aus mindestens vier im Rohzustand befindlichen keramischen Schichten gebildet ist, welche zusammengesintert werden, **dadurch gekennzeichnet, dass**
  - (a) die erste keramische Schicht (20) Kanäle (12, 14) aufweist zum Verteilen mindestens zweier, Chemikalien enthaltender Flüssigkeiten,
  - (b) die zweite keramische Schicht (30) eine Mischkammer (31) umfasst, die mit den Kanälen (12, 14) in Verbindung steht zum Mischen der die Chemikalien enthaltenden Flüssigkeiten,
  - (c) die dritte keramische Schicht (40) eine Reaktionskammer (44, 46, 48) aufweist, um die

Chemikalien in den Flüssigkeiten zur Reaktion zu bringen, und

(d) die vierte keramische Schicht (100) eine Analysekommer aufweist, die der Analyse des Ergebnisses der chemischen Reaktion dient, wobei die integrierte, mikrokeramische, chemische Anlage eine fünfte keramische Schicht (200) am Boden des unitären keramischen Körpers (10) umfasst sowie Mittel aufweist zum Transportieren der gemischten oder zur Reaktion gebrachten Chemikalien aus dem unitären keramischen Körper (10) heraus.

2. Integrierte mikrokeramische, chemische Anlage nach Anspruch 1, **gekennzeichnet durch** eine Wärmevorrichtung, die im unitären keramischen Körper (10) angeordnet ist, um diesen zu wärmen.
3. Integrierte mikrokeramische, chemische Anlage nach Anspruch 1, **dadurch gekennzeichnet, dass** die zweite, dritte, vierte und fünfte keramische Schicht Kapillare oder Kanäle mit kreisrundem Querschnitt aufweist.

2. Installation micro-chimique en céramique intégrée selon la revendication 1, comprenant en outre une unité de chauffage disposée dans le corps de céramique unitaire (10) destinée à chauffer un tel corps de céramique unitaire (10).
3. Installation micro-chimique en céramique intégrée selon la revendication 1, dans laquelle les seconde, troisième, quatrième et cinquième couches de céramique comprennent des capillaires ou des canaux de section transversale circulaire.

#### Revendications

1. Installation micro-chimique en céramique intégrée comportant un corps de céramique unitaire à couches multiples (10) formé à partir d'au moins quatre couches de céramique à l'état vert qui sont frittées ensemble comprenant :
  - (a) la première couche de céramique (20) qui est munie de passages (12, 14) destinés à distribuer au moins deux fluides contenant des produits chimiques,
  - (b) la seconde couche de céramique (30) comprenant une chambre de mélange (31) de seconde couche qui est en communication avec les passages (12, 14) destinée à mélanger les fluides contenant des produits chimiques,
  - (c) la troisième couche de céramique (40) contenant une chambre de réaction de troisième couche (44, 46, 48) destinée à faire réagir les produits chimiques dans les fluides, et
  - (d) la quatrième couche de céramique (100) comprenant une chambre d'analyse de quatrième couche destinée à une utilisation lors de l'analyse du résultat des réactions chimiques, dans laquelle l'installation micro-chimique en céramique intégrée comprend en outre une cinquième couche de céramique (200) se trouvant au niveau de la partie inférieure dudit corps de céramique unitaire (10) et définissant un moyen destiné à délivrer les produits chimiques mélangés ou ayant réagi vers la sortie depuis le corps de céramique unitaire (10).

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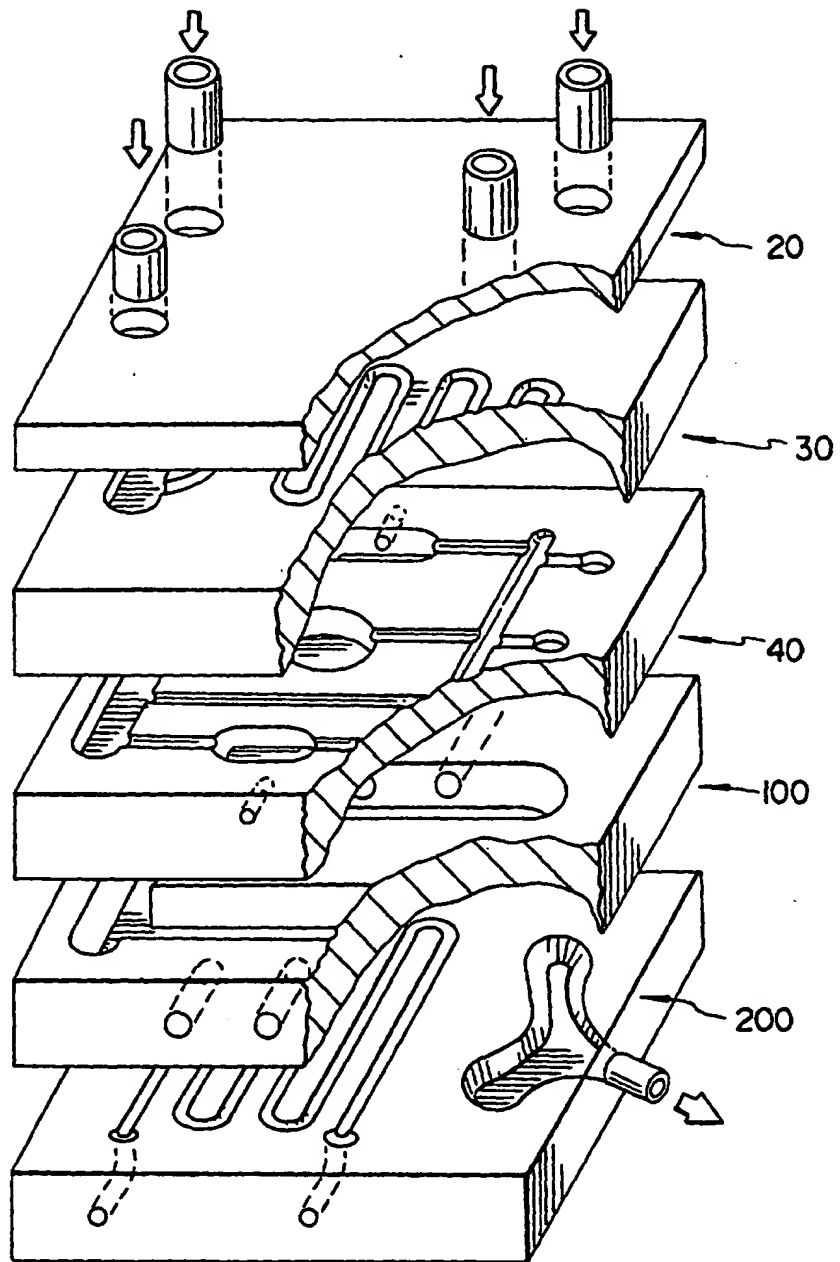
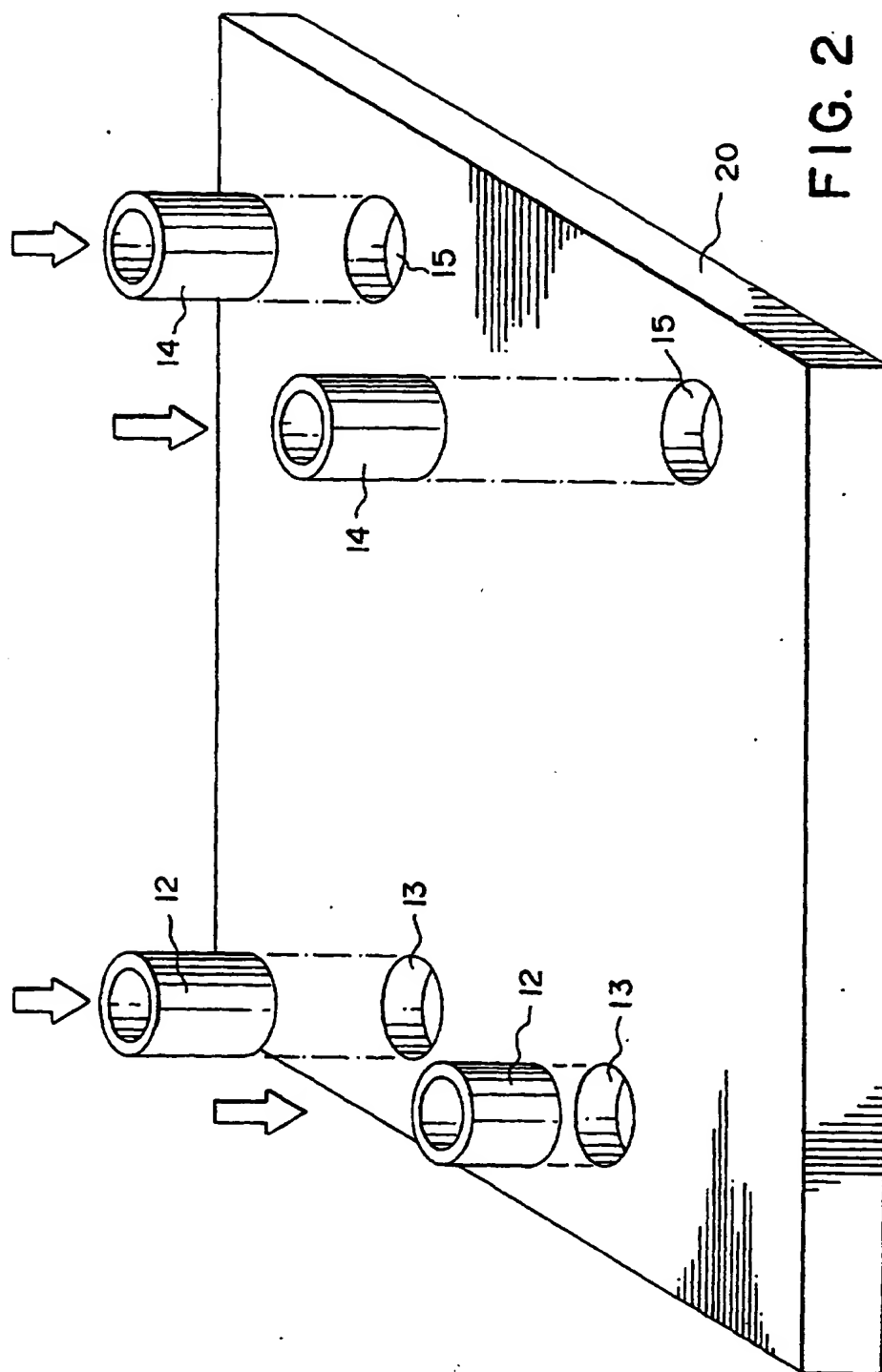


FIG. 1





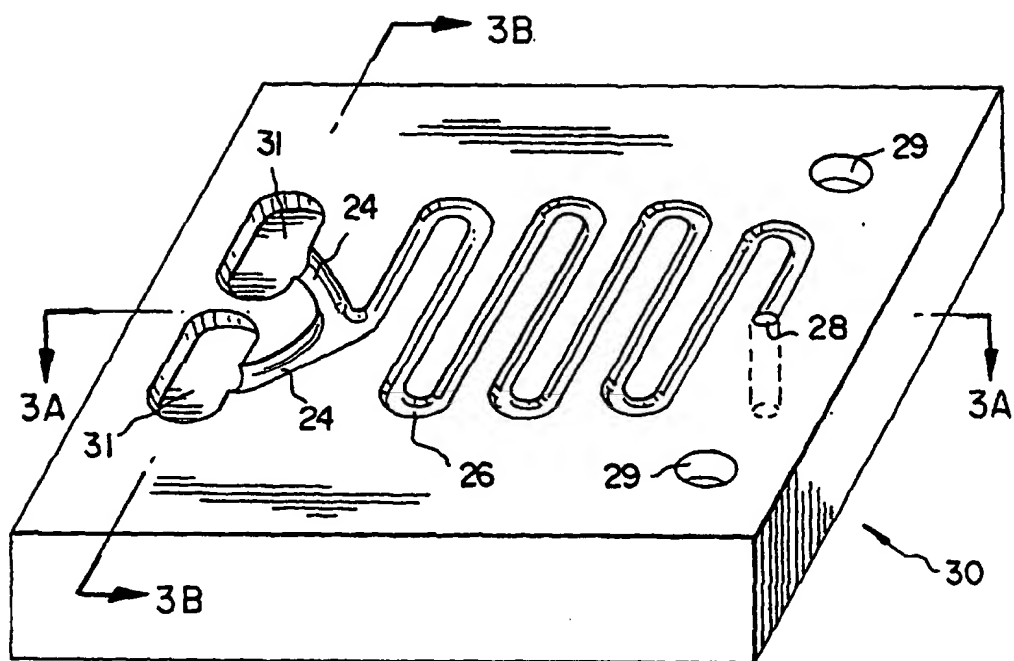


FIG. 3a

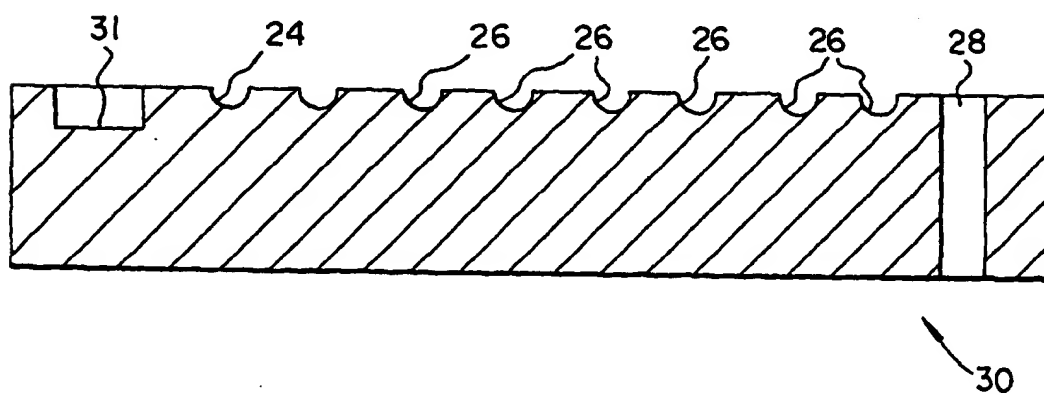
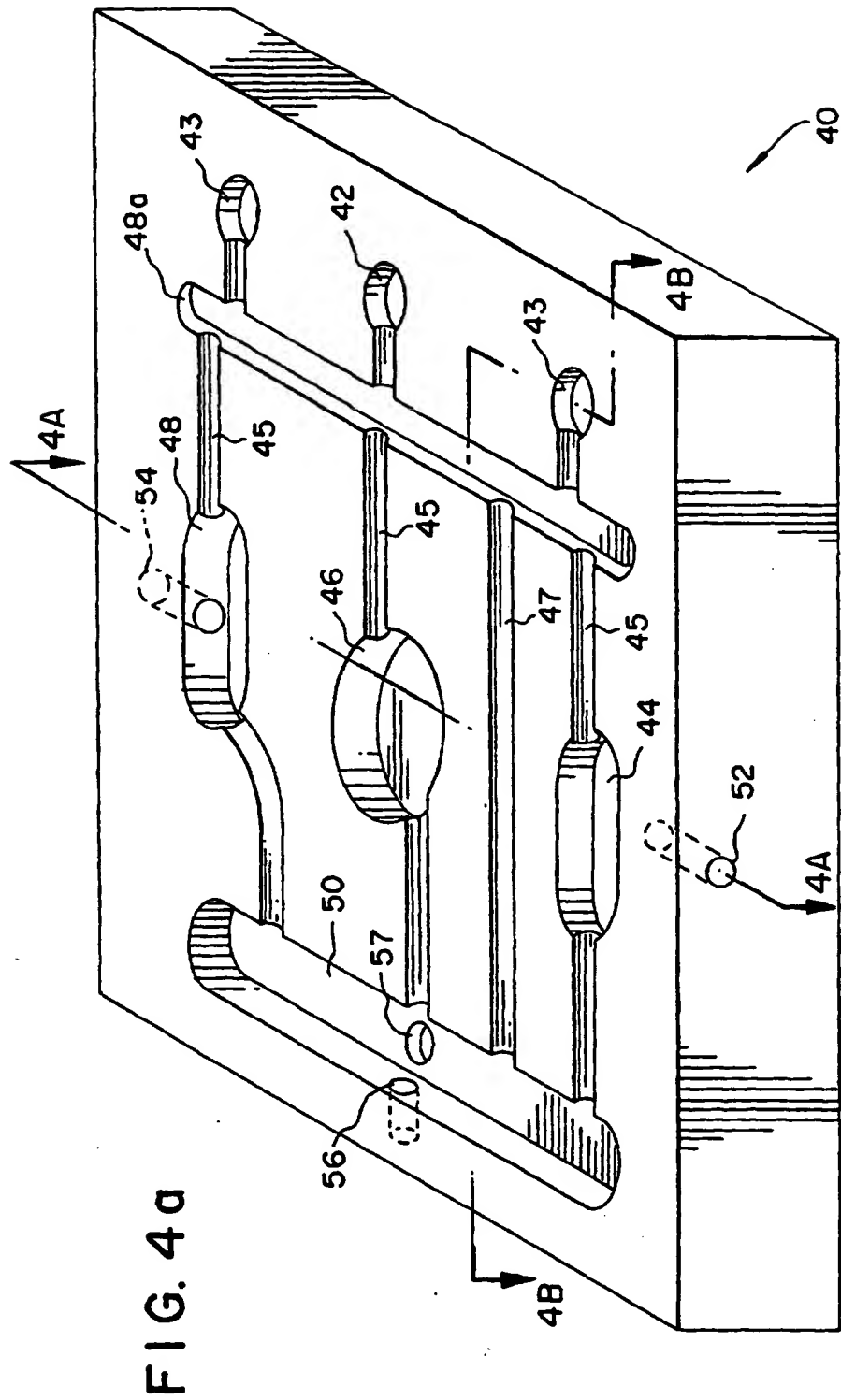


FIG. 3b



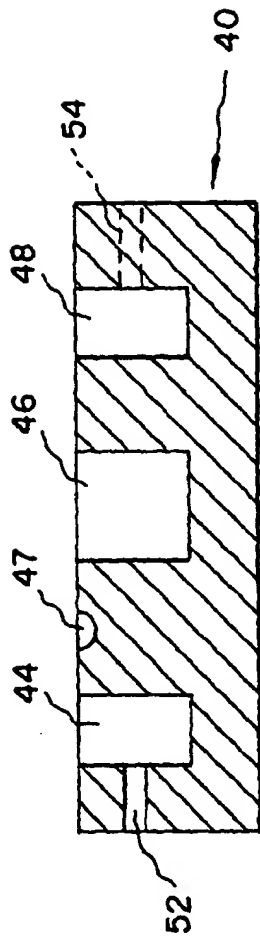


FIG. 4b

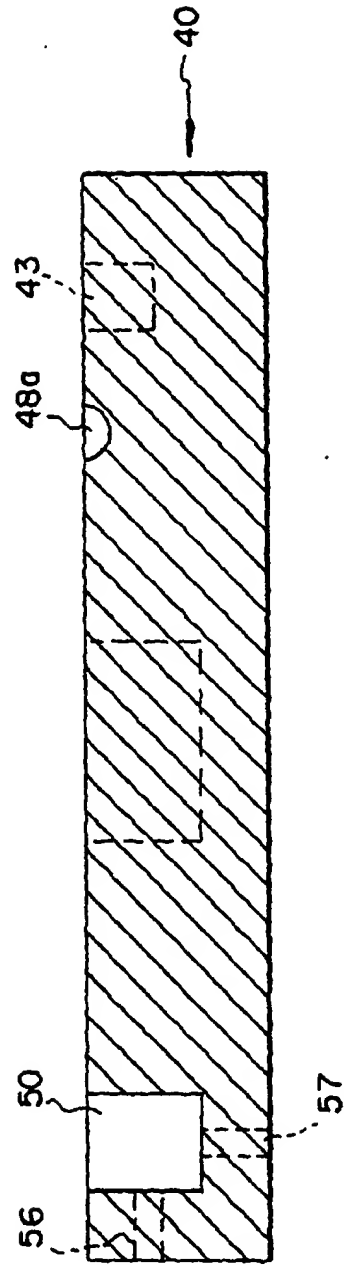


FIG. 4c

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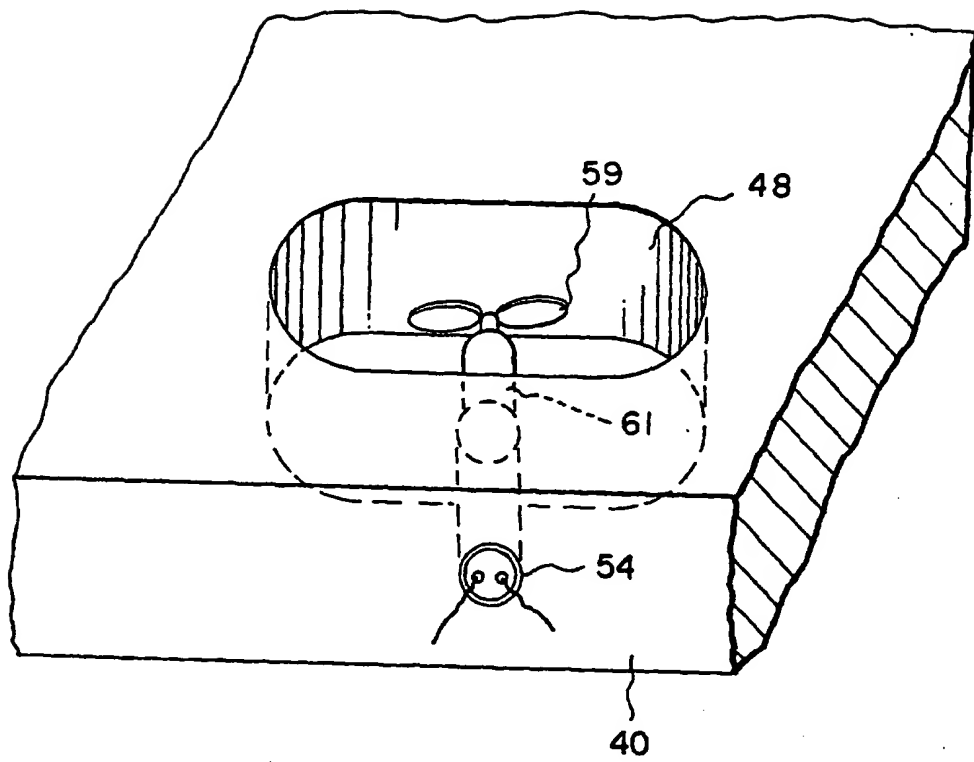


FIG. 5a

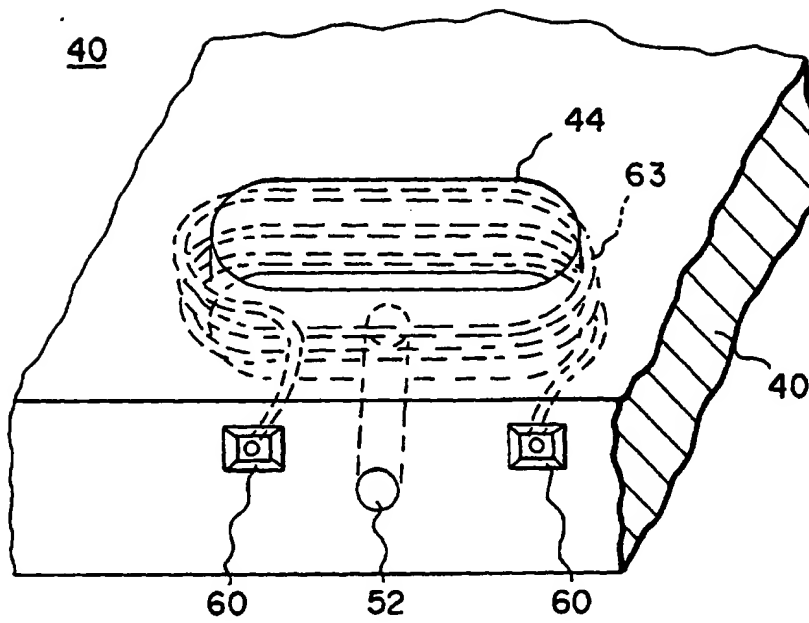


FIG. 5b

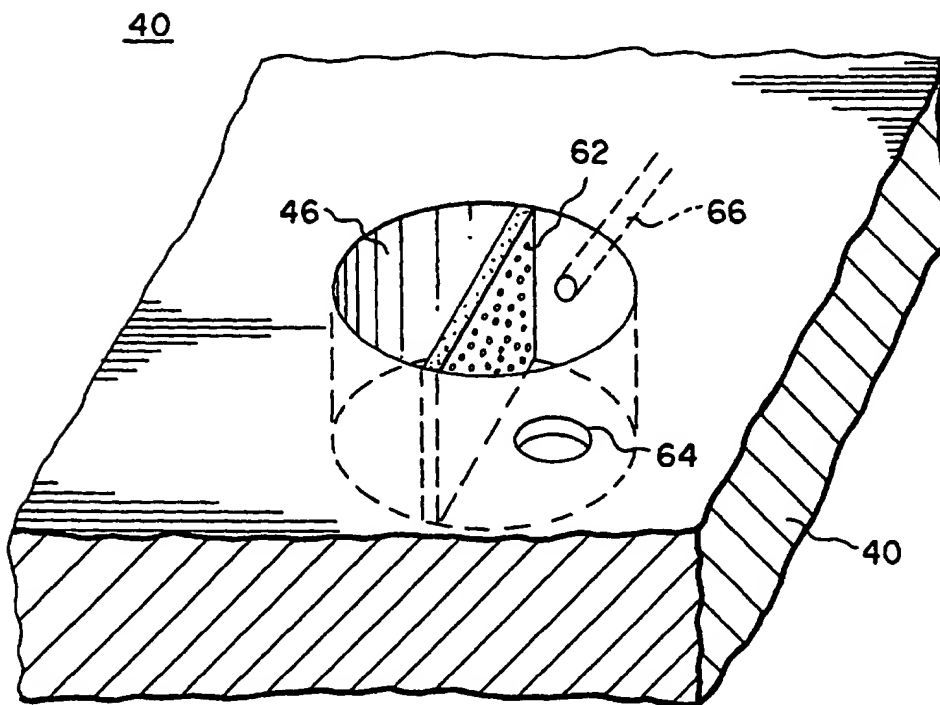


FIG. 5c

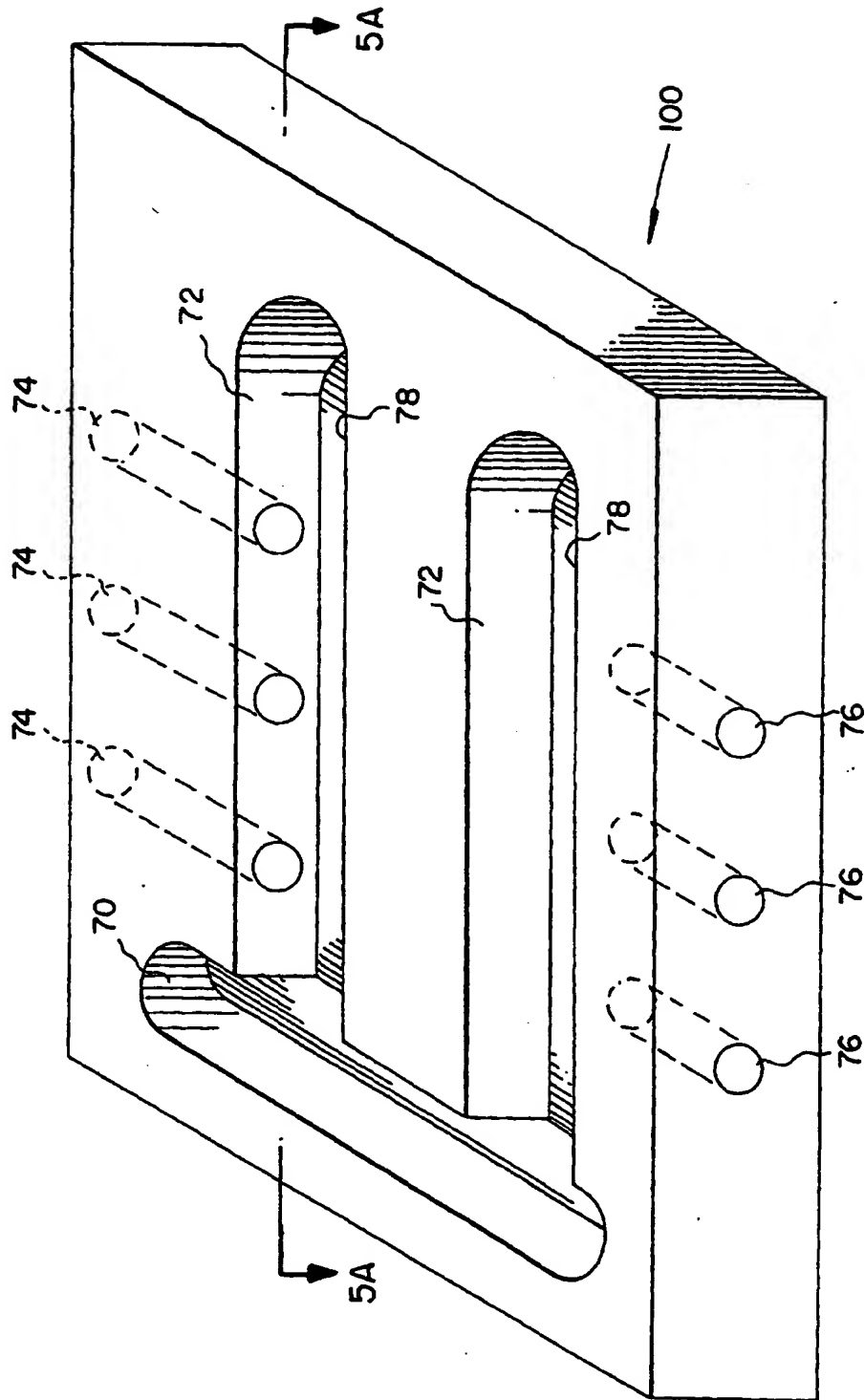


FIG. 6

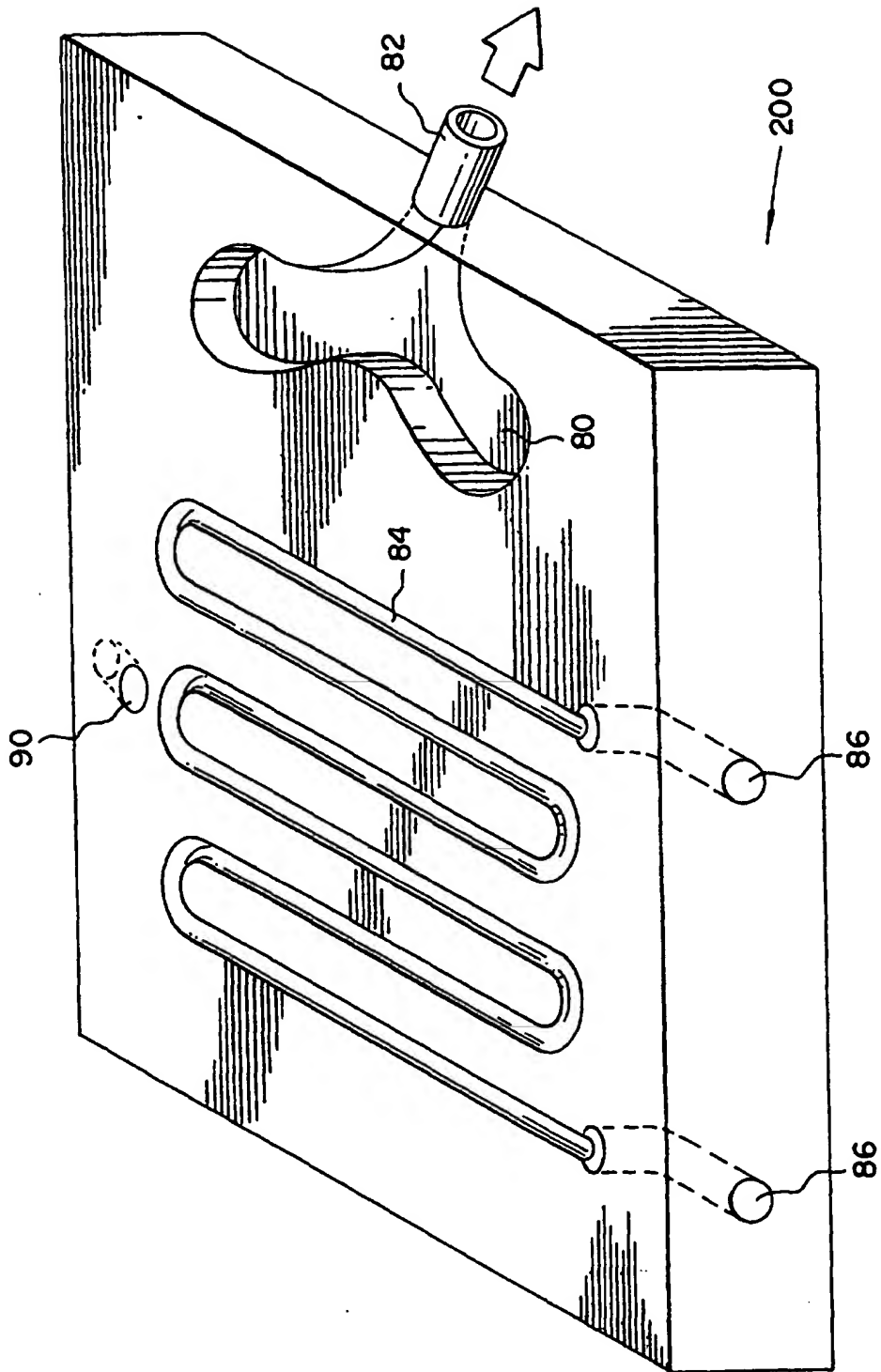


FIG. 7

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